



# Well Stimulation and Sand Production Management (PGE 489)

# Acid Types and Reactions with Different Rocks

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# What is Acidizing?

- Unsteady, non-isothermal, 3-D flow in porous media with chemical reactions
- Heterogeneous and homogeneous reactions
- Continuous variation in the porosity and permeability of the porous medium due to dissolution of the rock matrix and precipitation of the reaction products

# **Factors Affecting Acid Formula**

- Damage type and location
- Rock mineralogy
- Analysis of formation water
- Bottom hole temperature
- Well completion
- Well type
- OWC Line

# **Factors Affecting Acid Formula**

- Oil type (wax, asphaltenes)
- H<sub>2</sub>S content
- Reservoir pressure
- Permeability profile
- Water saturation

- Mineral acids
- Simple organic acids
- Mineral/organic acids
- Powder or solid acids
- Chelating agents
- In-situ generated acids

- Mineral acids
  - Hydrochloric acid (HCI)
  - Sulfuric acid (H<sub>2</sub>SO<sub>4</sub>)
  - Phosphoric acid (H<sub>3</sub>PO<sub>4</sub>)
  - Nitric acid (HNO<sub>3</sub>)

- Hydrochloric acid (HCI)
  - Cost effective
  - Available at 31 and 37 wt%
  - Ca, Mg chlorides are soluble
  - Fast reaction with calcite
  - Slower reaction with dolomite
  - Corrosive at high temp

- Hydrochloric acid (HCI)
  - Measure acid using titration
  - Colorless, slightly yellow/green
  - No impurities:
    - Iron
    - Sulfate
    - Phosphate
    - Fluoride

- Simple organic acids
  - More expensive
  - Mainly acetic and formic acids
  - Be careful with their salts
  - Less corrosive
  - With or without HCI
  - Reversible reactions
  - Requires especial corrosion inhibitors

- Simple organic acids
  - Contains COOH
  - Acetic acid (CH<sub>3</sub>COOH)
  - Formic acid (HCOOH)
  - Maximum concentration for acetic is 13 wt%
  - Maximum concentration for formic is 9 wt%
  - Mixture of HCI/organic acids
  - Mixture of formic/acetic

- Matrix acidizing design strongly depends on information about reservoir properties and formation damage.
- Acidizing process is complicated, and *no model can describe the process precisely*.
- In many cases stimulation results deviate from what is expected from design.

- *Matrix acidizing* is a well stimulation technique in which an acid solution is injected into the formation in order to dissolve some of the minerals present, and hence, recover or increase permeability in the near-wellbore vicinity.
  - Matrix Acidizing of Carbonate Reservoirs
- Matrix Acidizing of **Sandstone** Reservoirs





- The most common acids used in are hydrochloric acid (HCl), used to dissolve carbonate minerals, and mixture of hydrochloric and hydrofluoric acids (HCl/HF), for attacking silicate minerals such as clays and feldspars in Sandstone reservoir.
- Matrix acidizing is a near-wellbore treatment, with all of the acid reacting within about a **foot** of the wellbore in <u>Sandstone</u> <u>formation</u>, and within a few to perhaps **10 ft** of wellbore in <u>Carbonate</u>.



"The lack of a method to determine the depth of damage penetration by existing methods of well test analysis continues to make the acidizing of oil wells an inexact science"

J. L. Gidley (1970)

Q: What can we do to prevent "bad" acid treatments?

A: Monitor actual skin change during the injection.

- Evaluate acid systems
- Quantify damage removal
- Evaluate diversion process
- IMPROVE design for subsequent treatments

### **Field Examples**

### Example: Successful case *Pressure and injection rate record*



# Field Examples

Example: Successful case

Skin Evolution of Acidizing



# **Field Study Examples**

### Example-1:

### Reservoir properties

- reservoir pressure 8000 psi
- permeability100 md
- initial skin factor 35
- payzone thickness 138 ft
- well depth 11447 ft

### Treatment data

		No. stages	V (gal)
•	preflush	1	4957
•	main	1	9949
•	diversion	n/a	
•	spacer	2	5006

# **Field Study Examples**





### Example-1:

- Skin factor reduced from 35 to near zero
  - Production was doubled and drawdown was reduced from 1200 psi to 500 psi by the treatment
  - HCI did not remove the damage common in sandstone formation with low carbonate

# **Field Study Examples**

### Example-2:

### **Reservoir properties**

- reservoir pressure 1700 psi
- permeability
   150 md
- initial skin factor
- payzone thickness 54 ft
- well depth 3600 ft

### Treatment data

	No. stages	V (gal)
preflush	2	2095
main	2	4199
diversion	1	407
spacer	3	4000

# **Field Study Examples**

### Example-2:





### Example-2:

- The well did not respond as expected to the first acid injection
  - Sudden increasing of skin factor when diverter reached the perfs showed positive diversion effect
    - Two components of diversion effect on skin: filter cake build-up and viscous effect

# **Field Study Examples**

### Example-3:

### **Reservoir properties**

reservoir pressure3100 psipermeability150 mdinitial skin factor45payzone thickness132 ftwell depth7460 ft

### Treatment data

	No. stages	V (gal)
preflush	2	3444
main	2	7732
diversion	1	210
spacer	3	2289

# **Field Study Examples**

### Example-3:





### Example-3:

- Very successful stimulation in the first acid stage
- The second diversion stage could be eliminated since the second acid stage did not reduce skin factor any further

# **Fluid Chemistry**

• An acid is a compound that when dissolved in (or hydrolysed by) water, it releases hydrogen ions (H+) as the cation. Examples of commonly used acids are as follows:

Hydrochloric Acid.	HCI + H <sub>2</sub> O	$\rightarrow$	H⁺	+	CI
Hydrofluoric Acid.	HF + H <sub>2</sub> O	$\rightarrow$	H⁺	+	F <sup>-</sup>
Acetic Acid.	H <sub>3</sub> C-COOH + H <sub>2</sub> O	$\rightarrow$	H⁺	+	H <sub>3</sub> C-COO <sup>-</sup>
Formic Acid.	HCOOH + H <sub>2</sub> O	$\rightarrow$	H⁺	+	HCOO
Sulfamic Acid.	$H_2N-SO_2OH + H_2O$	$\rightarrow$	H⁺	+	H <sub>2</sub> N-SO <sub>3</sub> <sup>-</sup>
Water.	HOH + H <sub>2</sub> O	$\rightarrow$	H⁺	+	OH

#### A salts is a compound formed by the reaction of an acid with a base.

Sodium Chloride	HCI + NaOH	$\rightarrow$	NaCl + H <sub>2</sub> O
Calcium Chloride	2HCI + CaCO <sub>3</sub>	$\rightarrow$	$CaCl_2 + CO_2\uparrow + H_2O$
Silicon Tetrafluoride	4HF + SiO <sub>2</sub>	$\rightarrow$	SiF <sub>4</sub> + 2H <sub>2</sub> O
Barium Sulphate	$H_2SO_4$ + $Ba(OH)_2$	$\rightarrow$	$BaSO_4 + 2H_2O$
Magnesium Formate	2HCOOH + Mg(OH) <sub>2</sub>	$\rightarrow$	Mg(HCOO) <sub>2</sub> + 2H <sub>2</sub> O

## **Reaction Kinetics**

 Dissolving power expresses the amount of minerals that can be consumed by given amount of acid on a mass or volume basis.

• For reaction between 100% HCI and CaCO<sub>3</sub>:

$$\beta = \frac{v_{\text{mineral}} M W_{\text{mineral}}}{v_{acid}} = \frac{(1)(100.1)}{(1)(36.5)} = 1.37 \frac{Ib_m CaCO_3}{Ib_m HCl}$$

# **Reaction Kinetics**

• Volumetric Dissolving power (X) is defined as the volume of mineral dissolved by a given volume of acid, and related to gravimetric dissolving power by:

$$X = \beta \frac{\rho_{\text{acidsolution}}}{\rho_{\text{mineral}}} = \beta \frac{\rho_a}{\rho_m} \qquad \begin{cases} X = \text{volumetric dissolving power of acid solution,} \\ \mu_a = \text{density of acid, } \text{lb}_m/\text{ft}^3 \\ \rho_m = \text{density of mineral, } \text{lb}_m/\text{ft}^3 \end{cases}$$

For reaction between 15% HCl and  $CaCO_3$  with acid specific gravity of 1.07 and  $CaCO_3$  density of 169 Ib<sub>m</sub>/ft<sup>3</sup>, the volumetric dissolving power is:

$$X = ((0.15)(1.37)) \left( \frac{Ib_m CaCO_3}{Ib_m 15\% HCl} \right) \left( \frac{(1.07)(62.4) Ib_m 15\% HCl}{ft^3 15\% HCl} \left| \frac{ft^3 CaCO_3}{169 Ibm CaCO_3} \right) X = 0.082 \frac{ft^3 CaCO_3}{ft^3 15\% HCl}$$

# **Reaction Kinetics**

Table	Primary Chemical Reaction	ns in Acid Treatments
Montmoril	llonite (Bentonite)-HF/HCl:	$Al_4Si_8O_{20}(OH)_4 + 40HF + 4H^+ \leftrightarrow 4AlF_2^+ + 8SiF_4 + 24H_2O$
Kaolinite-I	HF/HCl:	$Al_4Si_8O_{10}(OH)_8 + 40HF + 4H^+ \leftrightarrow 4AlF_2^+ + 8SiF_4 + 18H_2O$
Albite-HF/	/HCl:	NaAlSi <sub>3</sub> O <sub>8</sub> + 14HF + 2H <sup>+</sup> $\leftrightarrow$ Na <sup>+</sup> + AlF <sup>+</sup> <sub>2</sub> + 3SiF <sub>4</sub> + 8H <sub>2</sub> O
Orthoclase	-HF/HCl:	$KAlSi_{3}O_{8} + 14HF + 2H^{+} \leftrightarrow K^{+} + AlF_{2}^{+} + 3SiF_{4} + 8H_{2}O$
Quartz-HF	F/HCl:	$SiO_2 + 4HF \leftrightarrow SiF_4 + 2H_2O$
		$SiF_4 + 2HF \leftrightarrow H_2SiF_6$
Calcite-HC	71:	$CaCO_3 + 2HCl \rightarrow CaCl_2 + CO_2 + H_2O$
Dolomite-l	HCl:	$CaMg(CO_3)_2 + 4HCl \rightarrow CaCl_2 + MgCl_2 + 2CO_2 + 2H_2O$
Siderite-H	Cl:	$FeCO_3 + 2HCl \rightarrow FeCl_2 + CO_2 + H_2O^2$

Dissolving Power of Various Acids						
Formulation	Acid	Q100	X			
Formulation		<b>p100</b>	5%	10%	15%	30%
Limestone	HCl	1.37	0.026	0.053	0.082	0.175
$CaCO_3$	НСООН	1.09	0.020	0.041	0.062	0.129
p=2.71 g/cm	СН3СООН	0.83	0.016	0.047	0.047	0.096
Dolomite	HCl	1.27	0.023	0.031	0.071	0.152
$MgCa(CO_3)_2$	НСООН	1.00	0.018	0.036	0.054	0.112
p=2.67 g/cm <sup>2</sup>	СН3СООН	0.77	0.014	0.027	0.041	0.083

# **Matrix Acidizing - Example**

In sand stone acidizing treatment, a preflush of HCl is usually injected ahead of the HF/HCl mixture to dissolve the carbonate minerals and establish a low-pH environment. A sandstone with a porosity of 0.20 containing 10% (volume) calcite (CaCO<sub>3</sub>) is to be acidized. If the HCl preflush is to remove all carbonate to a distance of 1 ft from the wellbore before HF/HCl stage enters the formation, what is the minimum preflush volume is required in gallons of acid solution per foot of formation thinness? The wellbore radius is 0.328 ft.



# **Matrix Acidizing - Solution**

The required minimum acid volume to dissolve all calcite is:

 $V_{acid} = V_{pore} + V_{to \ dissolve \ CaCO3} + V_{replaceCaCO3}$ The volume of acid needed to react with calcite (V<sub>m</sub>/X)

$$V_{m} = \pi (r_{HCl}^{2} - r_{w}^{2})(1 - \phi) x_{CaCO_{3}}$$

$$V_{m} = \pi (1.328^{2} - 0.328^{2})(1 - 0.20)(0.1) = 0.42 \text{ ft}^{3} / \text{ft} CaCO_{3}$$

$$\frac{V_{m}}{X} = \frac{0.42}{0.082} = 5.01 \text{ ft}^{3} \text{ HCl} / \text{ft}$$
The volume of pore space within 1 ft of wellbore is:
$$V_{p} = \pi (r_{HCl}^{2} - r_{w}^{2})\phi$$

$$V_p = \pi (1.328^2 - 0.328^2)(0.1) = 0.52 \text{ ft}^3 / \text{ft}$$

$$V_{HCl} = \frac{V_m}{X} + V_p + V_m = \frac{(5.01 + 0.52 + 0.42)ft^3}{ft} \left| \frac{7.48 \, gal}{ft^3} \right| = 44.5 \, gal / ft$$

- Acids were used to create wormholes to connect the formation to the wellbore
- Propagation of wormholes through the damaged zone yields negative skin
- Only a small fraction of the matrix must be dissolved



- A few large channels called wormholes form
- Structure of wormholes depends on many factors including:
  - Flow geometry
  - Injection rate
  - Reaction kinetics
  - Mass transfer rates

- Much larger than pores, hence insignificant pressure drop through them
- If the wormholes propagate through the damaged zone,

 $\mathbf{S} = -\ln(\mathbf{r}_{\rm wh}/\mathbf{r}_{\rm w})$ 

- Ex: 1.7 foot long wormholes propagating from a 6 inch radius well yield Skin of -1.22
- Wormhole structure depends on rock type, acid type, injection rate, temperature, ...

- Objective of acid stimulation was to create sufficiently long wormholes to give a post-treatment negative skin factor of -2 to -3.
- Injection rate may be limited by coiled tubing size
- Low injection rate resulted in compact dissolution of the formation face with no significant wormhole penetration
- The analysis can show that the skin factor did not change significantly throughout the entire treatment

- Acid selection based on:
  - reservoir depth (shallow or deep)
  - reservoir fracture gradient
  - reservoir permeability
  - Heterogeneity

# **Optimum Wormhole Condition**

### **Dissolution Patterns in Carbonate Acidizing**







a.

- 0.1 cc/min, face dissolution
- b. 0.2 cc/min, conical
- c. 1 cc/min, dominant
- d. 4.1 cc/min, ramified

# **Optimum Wormhole Condition**



### Dissolving Power: Gravimetric (β)

 $\beta = \frac{MW_{CaCO_3} \cdot \alpha_{CaCO_3}}{MW_{arid} \cdot \alpha_{acid}}$ 

 $CaCO_3 + 2HCI \qquad CaCI_2 + CO_2 + H_2O$ 

 $\beta_{100\%} = 100.1 * 1/(36.5 * 2) = 1.37$  lbmole CaCO<sub>3</sub>/lbmole HCl

**Volumetric** dissolving Power (X)

$$X = \beta rac{
ho_{acid}}{
ho_{CaCO_3}} \;\; {
m ft^3 \, CaCO_3/ft^3 \, HClc}$$

$$V_{acid} = V_{CaCO_3} / X$$

$$V_{CaCO_3} = \pi (r_{acid}^2 - r_w^2) (1 - \phi) x_{CaCO_3}$$
 ft<sup>3</sup> CaCO<sub>3</sub>/ft

Acid Capacity Number  $(N_{ac})$ : is the ratio of the amount of mineral dissolved by the acid occupying a unit volume of the rock pore space to the amount of mineral present in the unit volume of the rock

$$N_{ac,acid} = \frac{\phi \beta_{\%} \rho_{acid}}{(1-\phi)\rho_{rock}} = \frac{\phi X}{(1-\phi)}$$

Damköhler Number  $(N_{Da})$ : the ratio of reaction rate to convection rate

$$N_{Da} = \frac{\pi d_w L_w \kappa}{q}$$

 $d_w$  = wormhole radius, cm

 $L_w$  = wormhole length, cm

k = overall dissolution rate constant, cm/s

 $q = injection rate, cm^{3/s}$ 



Mahmoud and Nasr-El-Din, 2010, SPE 133497

The optimum Damköhler number was found to be 0.29, we can design the treatment based on that number

In the case of irreversible reactions (mass transfer):

$$\kappa = \frac{1.86 D_e^{2/3}}{d_w} \left(\frac{4q}{\pi L_w}\right)^{1/3}$$

Using these equations, the optimum flux can be estimated:

$$u_{opt} = \frac{130L_w D_e}{d_{core}^2}$$

- $u_{opt}$ = optimum flux, cm/s
- $L_w$  = wormhole length, cm
- $D_e = diffusion \ coefficient, \ cm^2/s$
- $d_{core}$  = core diameter, cm

From the previous equation the optimum injection rate can be determined:

$$Q_{opt} = 47.1 d_{core}^2 u_{opt}$$

 $Q_{opt} = optimum injection rate, cm<sup>3</sup>/min$  $d_{core} = core diameter, cm$ 

 $u_{opt} = optimum flux, cm/s$ 

To scale up the optimum injection rate to the field conditions the following equation can be used:

 $Q_{well} = Q_{core} \frac{r_{well} h_f}{r_{core} L_{core}}$ 

 $Q_{well}$  = optimum injection rate in the field,  $Q_{core}$  = optimum injection rate in the coreflood,  $r_{well}$  = well radius,  $h_{f}$  = reservoir thickness,  $r_{core}$  = core radius,

 $L_{core} = core length$ 

Different models can be used to predict for the wormhole radius:

$$r_{wh} = \left[\frac{bN_{ac}V}{\pi h\phi}D_e^{-2/3}\left(\frac{q}{h}\right)^{-1/3}\right]^{0.63}$$

Daccord et al., 1989

 $r_{wh}$  = wormhole penetration radius b = constant = 1.5 x 10<sup>-5</sup> in SI, N<sub>ac</sub> = acid capacity number, V = q \* t, D<sub>e</sub> = diffusion coefficient, h = formation thickness,

 $\phi$  = formation porosity,

To determine the volume of the acid per foot thickness of the formation the following formula can be used:

 $-\pi\phi D_e^{2/3}\left(\frac{q}{h}\right) r_{wh}^{1.6}$  $bN_{a}$ h

### Volumetric Model (Hill 1993):

- Assumes acid dissolves a constant fraction of rock volume penetrated
- Wormhole velocity is constant
- Assume fixed number of PV required to create a wormhole to a given distance

$$r_{wh} = \sqrt{r_w^2 + \frac{V}{\pi \phi h P V_{bt}}}$$

$$\frac{V}{h} = \pi \phi \left( r_{wh}^2 - r_w^2 \right) P V_{bt}$$

### **Example:**

Determine V/h (gal/ft) using different models for the following acid treatment:

- 15 wt% HCl,  $\rho_{acid} = 1.072$  g/cc
- Well radius = 6 in.
- Wormhole penetration = 3 ft
- Injection rate = 0.1 bpm/ft
- Diffusion coefficient =  $10^{-9} \text{ m}^2/\text{s}$
- Optimum flux = 0.18 cm/min
- Pore volume to breakthrough = 1.3 PV

### **Solution:**

$$N_{ac,acid} = \frac{\phi \beta_{\%} \rho_{acid}}{(1-\phi)\rho_{rock}} = 0.02$$

$$\frac{V}{h} = \frac{\pi \phi D_e^{2/3} \left(\frac{q}{h}\right)^{1/3} r_{wh}^{1.6}}{b N_{ac}} = 17.2 \ gal/ft \quad \text{Daccord}$$

$$\frac{V}{h} = \pi \phi \left( r_{wh}^2 - r_w^2 \right) P V_{bt} = 76.6 \, gal / ft \qquad \text{Volumetric}$$

# **Wormholing Rate**

# Buijse Model:

$$V_{wh} = W_{eff} v_i^{2/3} \left( 1 - e^{\left( -W_b v_i^2 \right)} \right)$$

$$v_i = \frac{q}{2\pi r h \phi} \qquad \qquad v_{i-opt} = \frac{q_{opt}}{2\pi r h \phi}$$

$$w_{eff} = \frac{v_{i-opt}^{1/3}}{PV_{bt-opt}} \qquad w_b = \frac{4}{v_{i-opt}^2}$$

### **Wormholing Rate**

Huang et al.(1989)

$$v_{wh} = v_{i,tip} \left(\frac{C_{tip}}{C_0}\right) N_{Ac}$$

 $v_{i,tip} = \frac{q}{2\pi \phi r_{wh}}$ 

Mahmoud and Nasr-El-Din (2011)

$$v_{wh} = \frac{4QN_{ac}}{\pi\phi d_{core}d_{wh}}$$

# **Wormholing Rate**

Wormholing rate can be used to determine the volume of the fluid required to create wormholes

Buijse 2005

$$PV_{bt} = \frac{d_{wh}}{d_{core}N_{ac}}$$

 $PV_{bt} = \frac{v_i}{v_{wh}}$ 

Mahmoud and Nasr-El-Din, 2011

Then the  $PV_{bt}$  can be used to determine the acid volume required for the treatment by the volumetric model

Optimum injection rate in acid treatment is the rate at which the dominant wormhole will be formed with the minimum acid volume



Optimum injection rate cannot be used in certain situations

$$Q_{\max} = \frac{2\pi h k \left(g_{fr} D_r - p_r\right)}{\mu \left(\ln \frac{r_e}{r_w} + S\right)}$$

Steady State FlowOpen HoleVertical Well

- Q<sub>max</sub> = maximum possible injection rate
- h = reservoir thickness
- k = reservoir permeability
- $g_{fr}$  = fracture gradient
- $D_r$  = reservoir depth
- $p_r$  = reservoir pressure
- $\mu = fluid \ viscosity$
- $r_e$  = reservoir drainage radius
- $r_w$  = wellbore radius
- S = damage skin

The maximum injection rate can be determined according to the reservoir and completion type

- Steady state, pseudo steady state, or transient flow
- Open hole, perforate, or slotted liner
- Vertical, inclined, or horizontal well

Scenario 1:  $Q_{opt} < Q_{max}$ , current stimulation fluid is safe to be used without the fear to frac the formation



Scenario 2:  $Q_{opt} > Q_{max}$ , current stimulation fluid is not safe, we have to look for alternatives

