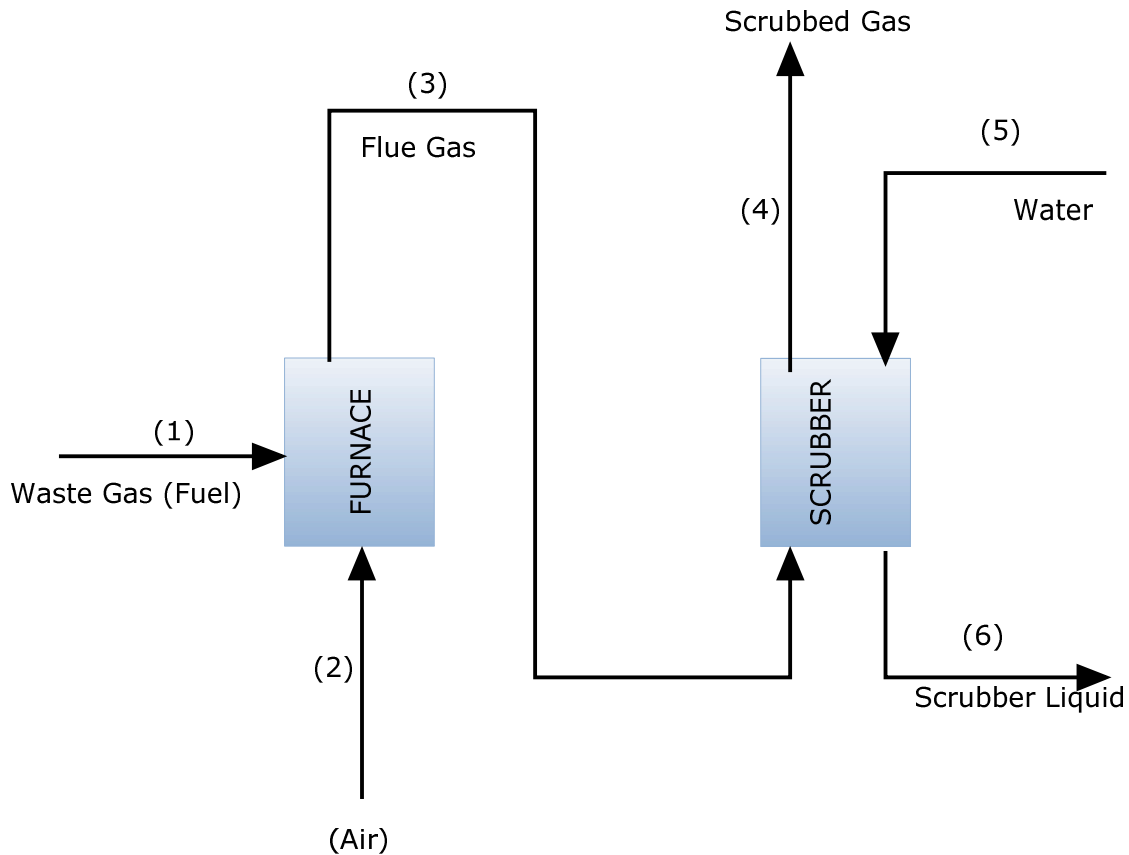


**CHE 302 Computerized Material and Energy Balances**  
**Solution to Tutorial (10)**

**Problem Statement**

**(Reklaitis G.V., "Introduction to Material and Energy Balances", Problem 4.21, page 257)**

A process waste gas containing  $H_2S$  is burned with air (see diagram below). A sample of 1.285 mol gas leaving the furnace is analyzed and found to contain 0.1 mol  $CO_2$  and 0.08 mol  $SO_2$ . Because of this high  $SO_2$  content, the flue gas is scrubbed with  $H_2O$ . The resulting scrubbed gas has a dry-basis analysis of 1.0%  $CO$ , 7.5%  $CO_2$ , 2.6%  $O_2$ , and 88.9%  $N_2$  and a water mole fraction of 1/11. The scrubber liquid consists of 1.5%  $CO_2$ , 8%  $SO_2$ , and the rest  $H_2O$ . If 10% excess air was used, calculate the fuel consumption. All compositions are in mole fractions or percent.



## SOLUTION

### **Basis: 1.285 mol gas leaving the furnace**

Solution strategy:

1. Check process degree of freedom on the basis of element balances. If the problem is correctly specified, then use element balances to solve the problem.
2. If the problem is underspecified on the basis of element balances, then construct a set of independent chemical reactions to represent the system and solve the problem using species balances.

First construct the atom matrix and then reduce it using the **array reduction procedure** operations.

The atom matrix is:

	CO	CO <sub>2</sub>	SO <sub>2</sub>	H <sub>2</sub> O	O <sub>2</sub>	CH <sub>4</sub>	H <sub>2</sub> S	
C	1	1	0	0	0	1	0	
O	1	2	2	1	2	0	0	→
S	0	0	1	0	0	0	1	
H	0	0	0	2	0	4	2	

	CO	CO <sub>2</sub>	SO <sub>2</sub>	H <sub>2</sub> O	O <sub>2</sub>	CH <sub>4</sub>	H <sub>2</sub> S	
C	1	1	0	0	0	1	0	
O	0	1	2	1	2	-1	0	→
S	0	0	1	0	0	0	1	
H	0	0	0	1	0	2	1	

	CO	CO2	SO2	H2O	O2	CH4	H2S
C	1	0	0	-1	-2	2	2
O	0	1	0	1	2	-1	-2
S	0	0	1	0	0	0	1
H	0	0	0	1	0	2	1

	CO	CO2	SO2	H2O	O2	CH4	H2S
C	1	0	0	0	-2	4	3
O	0	1	0	0	2	-3	-3
S	0	0	1	0	0	0	1
H	0	0	0	1	0	2	1

Therefore the elements C, O, S, H have independent balances.

Number of independent reactions = Number of species – Number of independent element balances

Number of species = 7

Number of independent element balances = 4

Number of independent reactions = 7 – 4 = 3 reactions.

Now we check the process degree of freedom on the basis of element balances:

	<b>Process</b>
Number of stream variables	22
Number of element balances	10
Number of compositions	3
Dry air relations (in stream 4)	3
Water mole fraction (in stream 4)	1
Percent excess air relation	1
Flows in stream 3	2
Basis	1
Degree of freedom	= 22 – 21 = 1

The problem is underspecified on the basis of element balances because the degree of freedom is greater than zero. We need to consider the species balances. We first have to construct a set of 3 independent chemical reactions. This set of reactions will be used to determine the degree of freedom on the basis of species balances. If the degree of freedom is zero, we then proceed to solve the problem using these three reactions in the material balances.

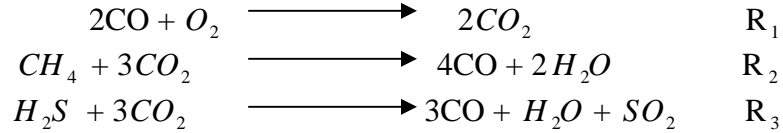
From the last reduced atom matrix the block of nonreduced columns (**C**) is:

$$\begin{array}{ccc} -2 & 4 & 3 \\ 2 & -3 & -3 \\ 0 & 0 & 1 \\ 0 & 2 & 1 \end{array}$$

Therefore the array  $\begin{pmatrix} -\mathbf{C} \\ \mathbf{I} \end{pmatrix}$ , where (I) is an identity matrix of size equal to the number of columns of **C**, is:

$$\begin{array}{cccc} \text{CO} & 2 & -4 & -3 \\ \text{CO}_2 & -2 & 3 & 3 \\ \text{SO}_2 & 0 & 0 & -1 \\ \text{H}_2\text{O} & 0 & -2 & -1 \\ \text{O}_2 & 1 & 0 & 0 \\ \text{CH}_4 & 0 & 1 & 0 \\ \text{H}_2\text{S} & 0 & 0 & 1 \end{array}$$

Therefore the set of the 3 independent chemical reactions which represent the system are:



Degree of freedom on the basis of species balances:

	Process
Number of stream variables	22+3
Number of species balances	14
Number of compositions	3
Dry air relations (in stream 4)	3
Water mole fraction (in stream 4)	1
Percent excess air relation	1
Flows in stream 3	2
Basis	1
Degree of freedom = 25 - 25 = ZERO	

**Variables Table:**

Stream Number	1	2	3	4	5	6	Total
Number of Independent Unknown variables	5	1	5	2	1	1	15+3♣ = 18
Selected Unknown Variables	$CH_4, CO, H_2S$ $O_2, N_2$	$O_2$	$CO, CO_2, SO_2$ $O_2, N_2$	$H_2O, CO$	$H_2O$	$H_2O$	

♣ Number of independent reactions = 3

**Number of independent unknowns = 18 variables**

Number of independent equations:

Species material balances = 14

Relations in stream 3 = 2

Water mole fraction relation in stream 4 = 1

Percent excess air relation = 1

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**Total = 18 equations**

**EZ Solve Computer Code:**

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 /\* Symbols: Water = W, Oxygen = O, Nitrogen = N, Hydrogen = H, Hydrogen disulfide = HS, Methane = CH, Sulfur dioxide = S, Carbon monoxide = C

Basis: 1.285 mol gas leaving the furnace\*/

//Furnace Material Balances:

$$\begin{aligned}0.0 &= CH1 - R2 && // CH_4 \text{ balance} \\C3 &= C1 - 2 * R1 + 4 * R2 + 3 * R3 && // CO \text{ balance} \\1.285 - (C3 + S3 + O3 + N3 + W3) &= 2 * R1 - 3 * R2 - 3 * R3 && // CO_2 \text{ balance} \\S3 &= 3 * R3 && // SO_2 \text{ balance} \\O3 &= O1 + O2 - R1 && // O_2 \text{ balance} \\N3 &= N1 + (79/21) * O2 && // N_2 \\0.0 &= HS1 - R3 && // H_2 S \text{ balance} \\W3 &= 2 * R2 + R3 && // H_2 O \text{ balance}\end{aligned}$$

//Scrubber Material Balances:

$$\begin{aligned}W4 + W6 &= W5 + W3 \\C4 &= C3 \\(7.5/1.0) * C4 + (2.5/89.5) * W6 &= 1.285 - (C3 + S3 + O3 + N3 + W3) \\(2.6/1.0) * C4 &= O3 \\(88.9/1.0) * C4 &= N3 \\(8.0/89.5) * W6 &= S3\end{aligned}$$

//Stream 3 relations:

$$\begin{aligned}1.285 - (C3 + S3 + O3 + N3 + W3) &= 0.1 && // CO_2 \text{ relation in stream 3} \\S3 &= 0.08 && // SO_2 \text{ relation in stream 3}\end{aligned}$$

//Stream 4 relation (the water mole fraction)

$$W4 = (1.0/11.0) * ((100.0/1.0) * C4 + W4)$$

//Percent excess relation

$$O2 = 1.1 * (0.5 * C1)$$

//Fuel consumption

$$\text{Fuel\_consumption} = CH1 + C1 + HS1 + O1 + N1$$

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Solution:

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$$\text{Fuel\_consumption} = 1.16937 \text{ moles}$$