

1. **Prediction of Effect of Process Variables on Drying Rate.** Using the conditions in Example 9.6-3 for the constant-rate drying period, do as follows.
- Predict the effect on R_C if the air velocity is only 3.05 m/s.
 - Predict the effect if the gas temperature is raised to 76.7°C and H remains the same.
 - Predict the effect on the time t for drying between moisture contents X_1 to X_2 if the thickness of material dried is 38.1 mm instead of 25.4 mm and the drying is still in the constant-rate period.

2. **Prediction in Constant-Rate Drying Region.** A granular insoluble solid material wet with water is being dried in the constant-rate period in a pan $0.61\text{ m} \times 0.61\text{ m}$ and the depth of material is 25.4 mm. The sides and bottom are insulated. Air flows parallel to the top drying surface at a velocity of 3.05 m/s and has a dry bulb temperature of 60°C and wet bulb temperature of 29.4°C . The pan contains 11.34 kg of dry solid having a free moisture content of 0.35 kg $\text{H}_2\text{O}/\text{kg}$ dry solid and the material is to be dried in the constant-rate period to 0.22 kg $\text{H}_2\text{O}/\text{kg}$ dry solid.
- Predict the drying rate and the time in hours needed.
 - Predict the time needed if the depth of material is increased to 44.5 mm.

3. **Graphical Integration for Drying in Falling-Rate Region.** A wet solid is to be dried in a tray dryer under steady-state conditions from a free moisture content of $X_1 = 0.40\text{ kg H}_2\text{O}/\text{kg}$ dry solid to $X_2 = 0.02\text{ kg H}_2\text{O}/\text{kg}$ dry solid. The dry solid weight is 99.8 kg dry solid and the top surface area for drying is 4.645 m^2 . The drying-rate curve can be represented by Fig. 9.5-1b.
- Calculate the time for drying using graphical integration in the falling-rate period.
 - Repeat but use a straight line through the origin for the drying rate in the falling-rate period.
- Ans. (a) $t(\text{constant rate}) = 2.91\text{ h}$, $t(\text{falling rate}) = 6.36\text{ h}$, $t(\text{total}) = 9.27\text{ h}$

4. **Drying Tests with a Foodstuff.** In order to test the feasibility of drying a certain foodstuff, drying data were obtained in a tray dryer with air flow over the top exposed surface having an area of 0.186 m^2 . The bone-dry sample weight was 3.765 kg dry solid. At equilibrium after a long period, the wet sample weight was 3.955 kg $\text{H}_2\text{O} + \text{solid}$. Hence, $3.955 - 3.765$, or 0.190, kg of equilibrium moisture was present. The following sample weights versus time were obtained in the drying test.

Time (h)	Weight (kg)	Time (h)	Weight (kg)	Time (h)	Weight (kg)
0	4.944	2.2	4.554	7.0	4.019
0.4	4.885	3.0	4.404	9.0	3.978
0.8	4.808	4.2	4.241	12.0	3.955
1.4	4.699	5.0	4.150		

- Calculate the free moisture content X kg $\text{H}_2\text{O}/\text{kg}$ dry solid for each data point and plot X versus time. (Hint: For 0 h, $4.944 - 0.190 - 3.765 = 0.989$ kg free moisture in 3.765 kg dry solid. Hence, $X = 0.989/3.765$.)
- Measure the slopes, calculate the drying rates R in $\text{kg H}_2\text{O}/\text{h} \cdot \text{m}^2$, and plot R versus X .
- Using this drying-rate curve, predict the total time to dry the sample from $X = 0.20$ to $X = 0.04$. Use graphical integration for the falling-rate period. What is the drying rate R_C in the constant-rate period and X_C ?